

PCTWORLD INTELLECTUAL PROPERTY ORGANIZATION
International Bureau

INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(51) International Patent Classification ⁶ : C08J 5/22, H01M 8/10	A1	(11) International Publication Number: WO 98/14505 (43) International Publication Date: 9 April 1998 (09.04.98)
(21) International Application Number: PCT/US97/17790 (22) International Filing Date: 29 September 1997 (29.09.97) (30) Priority Data: 60/027,169 1 October 1996 (01.10.96) US (71) Applicant (for all designated States except US): HOECHST CELANESE CORPORATION [US/US]; Robert L. Mitchell Technical Center, 86 Morris Avenue, Summit, NJ 07901 (US). (72) Inventors; and (75) Inventors/Applicants (for US only): SANSONE, Michael, J. [US/US]; 73 Cornell Avenue, Berkeley Heights, NJ 07922 (US). ONORATO, Frank, J. [US/US]; 23 Dryden Terrace, Phillipsburg, NJ 08865 (US). FRENCH, Stuart, M. [US/US]; 16 Lenape Trail, Chatham, NJ 07928 (US). MARIKAR, Faruq [US/US]; 2059 Algonquin Drive, Westfield, NJ 07090 (US). (74) Agents: KODROFF, Cathy, A. et al.; Howson and Howson, Spring House Corporate Center, 321 Norriston Road, Box 457, Spring House, PA 19477 (US).		(81) Designated States: AU, BR, CA, CN, JP, KP, KR, MX, US, European patent (AT, BE, CH, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE). Published <i>With international search report. Before the expiration of the time limit for amending the claims and to be republished in the event of the receipt of amendments.</i>
(54) Title: PROCESS FOR PRODUCING POLYMERIC FILMS FOR USE AS FUEL CELLS (57) Abstract A method for producing polymeric, e.g., polybenzimidazole (PBI) films, is provided by forming a porous membrane by coagulating a polymeric dope solution in a liquid coagulation bath containing a non-solvent alone or a mixture of a non-solvent and solvent; submerging the resulting membrane into a non-solvent bath to remove any residual solvent; placing the membrane into an acid solution, whereby the pores become filled with the acid solution; and drying the membrane to remove residual non-solvent which collapses the porous structure entrapping the acid and forming a dense film. An alternative method involves coagulating said polymer solution directly into an acid/solvent/non-solvent mixture to produce a porous membrane which imbibes the acid solution, followed by drying.		

FOR THE PURPOSES OF INFORMATION ONLY

Codes used to identify States party to the PCT on the front pages of pamphlets publishing international applications under the PCT.

AL	Albania	ES	Spain	LS	Lesotho	SI	Slovenia
AM	Armenia	FI	Finland	LT	Lithuania	SK	Slovakia
AT	Austria	FR	France	LU	Luxembourg	SN	Senegal
AU	Australia	GA	Gabon	LV	Latvia	SZ	Swaziland
AZ	Azerbaijan	GB	United Kingdom	MC	Monaco	TD	Chad
BA	Bosnia and Herzegovina	GE	Georgia	MD	Republic of Moldova	TG	Togo
BB	Barbados	GH	Ghana	MG	Madagascar	TJ	Tajikistan
BE	Belgium	GN	Guinea	MK	The former Yugoslav Republic of Macedonia	TM	Turkmenistan
BF	Burkina Faso	GR	Greece	ML	Mali	TR	Turkey
BG	Bulgaria	HU	Hungary	MN	Mongolia	TT	Trinidad and Tobago
BJ	Benin	IE	Ireland	MR	Mauritania	UA	Ukraine
BR	Brazil	IL	Israel	MW	Malawi	UG	Uganda
BY	Belarus	IS	Iceland	MX	Mexico	US	United States of America
CA	Canada	IT	Italy	NE	Niger	UZ	Uzbekistan
CF	Central African Republic	JP	Japan	NL	Netherlands	VN	Viet Nam
CG	Congo	KE	Kenya	NO	Norway	YU	Yugoslavia
CH	Switzerland	KG	Kyrgyzstan	NZ	New Zealand	ZW	Zimbabwe
CI	Côte d'Ivoire	KP	Democratic People's Republic of Korea	PL	Poland		
CM	Cameroon	KR	Republic of Korea	PT	Portugal		
CN	China	KZ	Kazakstan	RO	Romania		
CU	Cuba	LC	Saint Lucia	RU	Russian Federation		
CZ	Czech Republic	LI	Liechtenstein	SD	Sudan		
DE	Germany	LK	Sri Lanka	SE	Sweden		
DK	Denmark	LR	Liberia	SG	Singapore		
EE	Estonia						

PROCESS FOR PRODUCING POLYMERIC FILMS
FOR USE AS FUEL CELLS

5

Field of the Invention

This invention relates to the manufacture of films for use as polymer electrolytes in fuel cell applications.

10

Background of the Invention

Fuel cells can be configured in numerous ways with a variety of electrolytes, fuels and operating temperatures. For example, fuels such as hydrogen or methanol can be provided directly to the fuel cell electrode. Alternatively, fuels, such as methane or methanol, can be converted to a hydrogen rich gas mixture external to the cell itself and subsequently provided to the fuel cell. Air is the source of oxygen in most fuel cells, although in some applications, the oxygen is obtained by hydrogen peroxide decomposition or from a cryogenic storage system.

Although there are theoretically a limitless number of combinations of electrolyte, fuel, oxidant, temperatures and so on, practical systems include solid polymer electrolyte systems using hydrogen or hydrazine as the fuel source and pure oxygen as the oxidant. A polybenzimidazole (PBI) which has been doped with a strong acid is an example of a suitable solid polymer for use in an electrolyte system.

See, e.g., US Patent Nos. 5,091,087 which discloses a process for preparing a microporous PBI membrane having a uniform pore structure by immersing fine PBI particles in a polymeric solution of a high temperature

stable matrix polymer to coat the PBI with the matrix polymer, drying the coated PBI particle, and compression molding the particles to sinter the PBI. The matrix polymer is extracted from the molded PBI.

5 It is known in the art to imbibe polybenzimidazole (PBI) dense films with a strong acid to make a proton conducting media.

 Recently, International Patent Application No. WO96/13872, published May 9, 1996, disclosed a method of
10 doping a PBI with a strong acid, such as phosphoric acid or sulfuric acid, such that a single phase system is formed, i.e., acid is dissolved in the polymer.

 Even in view of the advances in the art, the performance, high cost and processability of suitable
15 polymeric electrolyte materials remain important considerations in fuel cell construction with respect to polymeric media for fuel cells.

Summary of the Invention

20 In one aspect, the present invention provides an improved method of preparing polymeric films and membranes, particularly those made of a PBI, for use as electrolytes in fuel cells. In one embodiment, the method comprises forming a porous structure by coagulating a PBI dope
25 solution in a coagulation bath containing a non-solvent alone or a mixture of a non-solvent and a solvent, both miscible in each other. The resulting membrane is then submerged into a water bath to remove any residual solvent, and then placed into an acid and water solution. The pores
30 are then filled with the acid/water mixture. The membrane is dried to remove residual water which collapse the porous structure entrapping the acid.

 In another aspect, the method comprises coagulating the polymer/solvent mixture directly in an

acid/solvent/water mixture to produce the membrane directly and imbibe the acid/water solution. The membrane is then dried to remove residual water and solvent and collapse the pores to produce a dense film. The amount of acid in the
5 resulting film can be controlled by adjusting the membrane porosity, which is determined by the solvent content in the coagulation medium, and controlling the acid concentration in the coagulation bath. Since PBIs are basic polymers, these compounds have an affinity for acids and retain them
10 under extreme conditions. This method is advantageous due to the speed of imbibition and the resulting morphology of the film produced.

In another aspect, the present invention provides improved porous polymeric films prepared by the
15 novel methods described herein. Such films are characterized by higher acid loadings and improved electrochemical and/or mechanical properties. For example, the films may be characterized by better retention of the acid than the films of the prior art.

20 Other aspects and advantages of the present invention are described further in the following detailed description of the preferred embodiments thereof.

Detailed Description of the Invention

25 The present invention provides an improvement over the art in methods of preparing a microporous polymeric film or membrane for use as an electrolyte in fuel cells. Generally, according to this process, polymeric films, preferably those made from a
30 polybenzimidazole (PBI), are prepared in a controlled fashion with single or multiple component liquids. In one embodiment, one of these liquids, the coagulation bath, comprises a non-solvent. In another embodiment, one of these liquids, the coagulation bath, comprises a miscible

mixture of a non-solvent and a solvent. In still a further embodiment, one of these liquids, the coagulation bath, comprises a miscible mixture of a non-solvent, a solvent and an acid.

5 According to the methods of this invention, a porous structure is formed by coagulating polymer dope solutions in a coagulation bath containing either a non-solvent alone, or a miscible mixture of a solvent and a non-solvent. The addition of a solvent to the mixture
10 slows down the coagulation reaction and can change the morphology of the resulting membrane. The resulting membrane is then submerged into a bath containing the non-solvent to remove any residual solvent, and then placed into a solution containing an acid and a non-solvent, such
15 as an acid/water solution or an acid/methanol solution, among other non-solvents, to fill the membrane pores with the acid solution. The membrane is oven dried to remove residual non-solvent which collapses the porous structure, entrapping the acid.

20 An advantage of this method is that the acid imbibition occurs over a short timespan, i.e., about 30 seconds to about 1 hour, in contrast to prior art methods which take between 10 to 72 hours. This advantage is reflected in both reduced cost and better performance of
25 the electrolyte.

 In any of the embodiments of the method which are described in the examples and in more detail below, the term "polymer dope solution" means a solution containing about 2 to about 30% of a selected polymer dissolved in a
30 suitable solvent. Suitable solvents in which the polymers are dissolved include, without limitation, DMAC, NMP, DMF, DMSO, strong acids such as sulfuric acid, methanesulfonic acid, and trifluoroacetic acid.

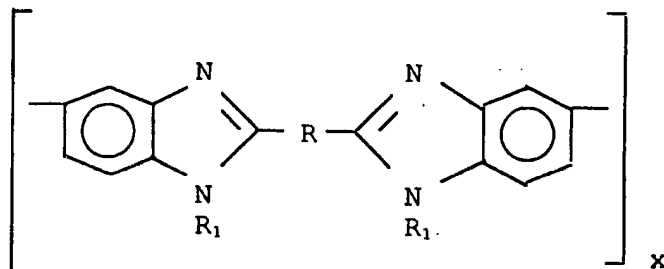
The selected polymers employed to form the dopes include polymers containing basic groups that can form complexes with stable acids, or polymers containing acidic groups which can be used to form films suitable for use as a solid polymer electrolyte membrane in fuel cells. These polymers may contain a variety of functional groups. Examples of such polymers include, but are not limited to, polybenzimidazoles (PBI), poly(pyridines), poly(pyrimidines), polyimidazoles, polybenzthiazoles, polybenzoxazoles, polyoxadiazoles, polyquinoxalines, polythiadiazoles, and poly(tetrazapyrenes). The presently preferred, and exemplified polymers are PBIs.

The polybenzimidazole polymer has the known structure, wherein R and R¹ are selected from among a variety of linking or functional groups [See, e.g., US Patent Nos. 4,814,399 and 5,525,436; and International Patent Application No. WO96/13872]:

20

25

30



More specifically, in a desired embodiment of this method of producing a polymeric microporous film, polymer dope solution is coagulated in a coagulation bath comprising a non-solvent alone. Among such non-solvents are included, without limitation, water, methanol, acetone, other alcohols and other water miscible non-solvents. The amount of non-solvent(s) in the bath is about 100% by weight of the composition. The bath temperature is

generally room temperature but can be anywhere between the freezing point and boiling point of the non-solvent.

The polymeric dope is coagulated in the non-solvent bath until it coagulates into a porous membrane, characterized by a porous structure. The coagulation time, i.e., the amount of time taken for the polymer dope to coagulate, is generally between about 5 seconds to 1 hour.

In still another desired embodiment of this method of producing a polymeric microporous film, polymer dope solution is coagulated in a coagulation bath comprising a mixture of a solvent and a non-solvent. Suitable solvents include, without limitation, DMAC, NMP, DMF, DMSO, strong acids such as sulfuric acid, methanesulfonic acid, trifluoroacetic acid and triflic. From among the solvents and non-solvents identified above, the following combinations are preferred: DMAC/methanol, NMP/methanol, DMAC/water. However, any combination of solvents and non-solvents which are miscible in each other will work in the method of this invention.

Generally, in this embodiment of the method of this invention, the amount of solvent and non-solvent in the bath is between about 0% and about 90% by weight of the solvent, and between about 100% and about 10% by weight of the non-solvent. The bath temperature is generally room temperature, but can be anywhere between the freezing point and boiling point of the non-solvent/solvent mixture. The polymeric dope is precipitated in the coagulation bath for about 5 seconds to about 1 hour until it coagulates into a porous membrane, characterized by a porous structure.

The amount of solvent or non-solvent in the coagulation bath controls the kinetics of the reaction, and thereby controls the morphology of the resulting film. The greater the amount of solvent in the bath, the slower the

coagulation occurs. For example, at a DMAC content of 50% by weight, a PBI dope solution coagulates at about 3 minutes.

After soaking in one of the above-discussed
5 coagulation baths, the resulting membrane is submerged into a non-solvent bath, such as a water or methanol, or a bath formed of a mixture of non-solvents to remove any residual solvent for about 0.5 to about 60 minutes, usually less
10 than about 5 minutes. The bath temperature is generally room temperature but can be anywhere between the freezing point and boiling point of the non-solvent.

The membrane is then soaked in an acid solution consisting of acid and a non-solvent, for example a solution of acid and water, or acid and methanol, among
15 others. The acid solution generally contains about 5 to about 100 weight percent, preferably about 50 weight percent, of an acid, such as phosphoric, sulfuric, methanesulfonic acids, among others. Generally the acid solution is at room temperature, with elevated temperatures
20 increasing the rate of imbibition. This soaking step generally takes about 1 minute to about 2 hours. The preferred time depends on temperature and acid concentration. For example, at room temperature and 50 weight% acid, the soaking step takes less than about 5
25 minutes, in which time the pores in the coagulated membrane become filled with the acid solution.

The membrane is then dried at room temperature to about 200°C, preferably between about 80°C to about 180°C, to remove residual solvent and non-solvent, such as
30 DMAC, water, and/or methanol. This drying step collapses the porous structure, thereby entrapping the acid and forming a dense film. The resulting membrane or film is

capable of imbibing up to about 80% of the acid in the acid solution.

In an alternative embodiment of the method of this invention, the polymer dope is precipitated directly
5 in a coagulation bath consisting of a mixture of a non-solvent and an acid, or a non-solvent, a solvent and an acid, the components of the bath being miscible in each other. This allows the production of the acid imbibed membrane in a single step, i.e., without a separate soaking
10 step. The individual components of the coagulation bath are selected from the lists of solvents, non-solvents and acids described above.

The coagulation bath containing an acid and a non-solvent generally comprises about 5 to about 75% by
15 weight of a suitable strong acid, selected from among those acids discussed above, in admixture with between about 95 to about 25% by weight non-solvent. The coagulation bath containing an acid, a solvent and a non-solvent generally comprises between about 5 to about 75% by weight of a
20 suitable strong acid, between about 95 to about 10% by weight non-solvent, and between 0 to about 85% by weight solvent. These mixtures are usually at room temperature, but can be up to 80°C. The polymer from the coagulation bath is placed in this mixture for between about 1 and
25 about 60 minutes. In this bath the pores of the coagulated membrane become filled with the acid solution.

The membrane is then dried at room temperature to about 200°C, preferably between about 80°C to about 180°C for about 5 minutes to about 24 hours depending on drying
30 conditions. The drying removes residual solvent and non-solvent, such as DMAC, water, and/or methanol, and collapses the pores to entrain the acid and produce a dense film.

In any embodiment of the method of this invention, the amount of acid in the resulting film can be controlled by adjusting the membrane porosity, temperature, soak time, and acid concentration as well as the specific materials employed. By controlling the acid concentration in the acid bath and the residence time, one controls the amount of acid in the resulting film. Since PBI is a basic polymer, it has an affinity for acids and will retain then under extreme conditions.

According to these methods, dense films or asymmetric membranes may be prepared in a controlled fashion, more rapidly than the prior art. These methods lead to better functional and mechanical properties of the film. Among such functional properties is a more tenacious acid retention, better electrochemical properties, and possibly other enhanced properties desirable for fuel cell use. The polymeric membranes resulting from the practice of these methods will generally contain from about 40% to about 80% acid by weight of the membrane itself. For a polymer to function adequately as an electrolyte in a fuel cell, about 50% or more acid is required.

The following examples illustrate the preferred compositions and methods of the invention, using a PBI as the exemplified polymer. These examples are illustrative only and do not limit the scope of the invention.

Example 1 - PBI Cast Films with Non-Solvent Coagulation Bath

PBI plate glass cast films (20 mil thickness wet cast) using an adjustable casting knife are prepared as follows. The polymeric dope solution (Sample 23-1) is prepared by mixing 10g PBI (10% solids) [poly 2,2'-(metaphenylene)-5,5'-bibenzimidazole, Hoechst Celanese Corporation] and 90g DMAC [DuPont]. This dope solution is

then placed in a 100% by weight water coagulation bath for coagulation of the polymer dope into a membrane. After 3 minutes in the bath, the membrane was removed and rinsed in a water bath for 1 minute at 23°C.

- 5 In a second step, the membrane is then soaked in an aqueous acid solution containing 85% phosphoric acid. This soaking occurs at a temperature of 23°C for about 2 minutes. The membrane is then oven dried at a temperature of 120°C for 12 hours to remove residual water and solvent,
10 e.g., DMAC. The resulting dense film contains about 52% acid by weight.

Example 2 - PBI Cast Films with Non-Solvent Coagulation Bath

- 15 PBI plate glass cast films (20 mil thickness wet cast) using an adjustable casting knife are prepared as follows. The polymeric dope solution (Sample 23-1) is prepared by mixing 10g PBI (10% solids) [poly 2,2'-(metaphenylene)-5,5'-bibenzimidazole, Hoechst Celanese
20 Corporation] and 90g DMAC [DuPont]. This solution is then placed in a coagulation bath containing 100% by weight methanol. After 6 minutes in the bath, the membrane was removed and rinsed in a methanol bath for 3 minutes at 23°C.

- 25 In the second step, the membrane is then soaked in a methanol/acid solution containing 50% phosphoric acid. This soaking occurs at a temperature of 23°C for 5 minutes. The membrane is then oven dried at a temperature of 120°C for 12 hours to remove residual methanol and DMAC.
30 The resulting dense film contains about 58% acid by weight. The resulting membrane has improved acid retention and better mechanical properties.

Example 3 - PBI Cast Films with a Non-Solvent/Solvent
Coagulation Bath

PBI plate glass cast films (20 mil thickness wet cast) using an adjustable casting knife are prepared as follows. The polymeric dope solution (Sample 23-1) is prepared by mixing 10g PBI (10% solids) [poly 2,2'-(metaphenylene)-5,5'-bibenzimidazole, Hoechst Celanese Corporation] and 90g DMAC [DuPont]. This solution is then placed in a coagulation bath containing both a non-solvent and a solvent, i.e., 50/50 wt% methanol/DMAC. After 4 minutes in the bath, the membrane was removed and rinsed in a methanol bath for 5 minutes at 23°C.

In the second step, the membrane is then soaked in a methanol/acid solution containing 60% phosphoric acid. This soaking occurs at a temperature of 23°C for 10 minutes. The membrane is then oven dried at a temperature of 140°C for 14 hours to remove residual methanol and DMAC. The resulting dense film contains about 61% acid by weight. The resulting membrane also has improved acid retention and better mechanical properties.

Example 4 - PBI Cast Films with Single Step
Coagulation/Acid Bath

PBI plate glass cast films (20 mil thickness wet cast) using an adjustable casting knife are prepared as follows. The polymeric dope solution (Sample 23-1) is prepared by mixing 10g PBI (10% solids) [poly 2,2'-(metaphenylene)-5,5'-bibenzimidazole, Hoechst Celanese Corporation] and 90g DMAC [DuPont]. According to the single step embodiment of the method of this invention, this dope solution is then placed in a single non-solvent/solvent/acid bath for both coagulation and acid imbibition. This bath contains 30/20/50 wt%

methanol/DMAC/phosphoric acid bath. After 8 minutes in the bath, the membrane was removed. The membrane is then oven dried at a temperature of 60°C for 2 hours, 100°C for 2 hours, and 150°C for 10 hours to remove residual methanol
5 and DMAC. The resulting dense film contains about 70% acid by weight.

All documents cited above are incorporated by reference. Numerous modifications and variations of the
10 present invention are included in the above-identified specification and are expected to be obvious to one of skill in the art. Such modifications and alterations to the compositions and processes of the present invention are believed to be encompassed in the scope of the claims
15 appended hereto.

WHAT IS CLAIMED IS:

1. A method for producing a polymeric film suitable for use as an electrolyte comprising the steps of:
 - a. forming a porous membrane by coagulating a polymer dope solution, said solution comprising a polymer dissolved in a selected solvent, in a liquid coagulation bath comprising a non-solvent;
 - b. submerging the resulting membrane into a non-solvent bath to remove any residual solvent;
 - c. placing said membrane into an acid solution in a non-solvent, whereby the pores become filled with the acid solution;
 - d. drying the membrane to remove residual non-solvent, which collapses the porous structure entrapping the acid and forming a dense film.
2. The method according to claim 1 wherein said polymer dope solution comprises a solution containing about 2 to about 30% of a selected polymer dissolved in about 98 to about 70% of a suitable solvent.
3. The method according to claim 2 wherein said selected polymer is selected from the group consisting of a polybenzimidazole (PBI), a poly(pyridine), a poly(pyrimidine), a polyimidazole, a polybenzthiazole, a polybenzoxazole, a polyoxadiazole, a polyquinoxaline, a polythiadiazole, and a poly(tetrazapyrene).
4. The method according to claim 2 wherein said polymer is a PBI.

5. The method according to claim 1 wherein said non-solvent is selected from the group consisting of water, methanol, acetone, alcohols and water miscible non-solvents.

6. The method according to claim 1 wherein said coagulation bath further comprises a solvent.

7. The method according to claim 6 wherein said solvent is selected from the group consisting of DMAC, NMP, DMF, DMSO, sulfuric acid, methanesulfonic acid, trifluoroacetic acid and triflic.

8. The method according to claim 1 wherein said coagulation bath comprises a miscible mixture of a non-solvent and a solvent.

9. The method according to claim 8 wherein said mixture is selected from the groups consisting of DMAC and methanol, NMP and methanol, and DMAC and water.

10. The method according to claim 1 wherein said acid solution comprises between about 5 to about 100 weight percent of an acid and about 95% to 0% non-solvent.

11. The method according to claim 10 wherein said acid solution comprises about 50% acid and 50% non-solvent.

12. The method according to claim 10 wherein said acid is selected from the group consisting of phosphoric, sulfuric, and methanesulfonic acids.

13. A porous polymeric film produced by the method of any of claims 1-12.

14. A method for producing polymeric films suitable for use as an electrolyte comprising the steps of:

a. adding a polymeric dope solution, said solution comprising a polymer dissolved in a selected solvent, in a liquid coagulation bath comprising a non-solvent and an acid, wherein the dope solution coagulates into a membrane which imbibes acid; and

b. drying the membrane to remove residual non-solvent, which collapses the porous structure entrapping the acid and producing a dense film.

15. The method according to claim 14 wherein said polymer dope solution comprises a solution containing about 2 to about 30% of a selected polymer dissolved in about 98 to about 70% of a suitable solvent.

16. The method according to claim 15 wherein said selected polymer is selected from the group consisting of a polybenzimidazole (PBI), a poly(pyridine), a poly(pyrimidine), a polyimidazole, a polybenzthiazole, a polybenzoxazole, a polyoxadiazole, a polyquinoxaline, a polythiadiazole, and a poly(tetrazapyrene).

17. The method according to claim 15 wherein said polymer is a PBI.

18. The method according to claim 14 wherein said non-solvent is selected from the group consisting of water, methanol, acetone, alcohols and water miscible non-solvents.

19. The method according to claim 14 wherein said coagulation bath further comprises a solvent.

20. The method according to claim 19 wherein said solvent is selected from the group consisting of DMAC, NMP, DMF, DMSO, sulfuric acid, methanesulfonic acid, trifluoroacetic acid and triflic.

21. The method according to claims 14 wherein said acid is selected from the group consisting of phosphoric acid, sulfuric acid, and methanesulfonic acid.

22. The method according to claim 14 wherein the liquid coagulation bath contains between about 5% to 75% by weight acid and between about 95% to about 25% non-solvent.

23. The method according to claim 19 wherein the liquid coagulation bath contains between about 5% to 75% by weight acid, between about 95% to about 10% non-solvent, and between 0 to 85% solvent.

24. A porous polymeric film produced by the method of any of claims 14-23.

INTERNATIONAL SEARCH REPORT

Intern. Application No

PCT/US 97/17790

A. CLASSIFICATION OF SUBJECT MATTER
IPC 6 C08J5/22 H01M8/10

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC 6 C08J H01M

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	WO 96 13872 A (UNIV CASE WESTERN RESERVE) 9 May 1996 cited in the application see the whole document ---	1-24
A	US 4 664 761 A (ZUPANCIC JOSEPH J ET AL) 12 May 1987 see the whole document ---	1-24
A	US 4 693 824 A (SANSONE MICHAEL J) 15 September 1987 see the whole document ---	1-24
P,A	US 5 599 639 A (SANSONE MICHAEL J ET AL) 4 February 1997 -----	

☐ Further documents are listed in the continuation of box C.

☒ Patent family members are listed in annex.

* Special categories of cited documents :

"A" document defining the general state of the art which is not considered to be of particular relevance

"E" earlier document but published on or after the international filing date

"L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)

"O" document referring to an oral disclosure, use, exhibition or other means

"P" document published prior to the international filing date but later than the priority date claimed

"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention

"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone

"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.

"&" document member of the same patent family

Date of the actual completion of the international search

5 February 1998

Date of mailing of the international search report

18/02/1998

Name and mailing address of the ISA

European Patent Office, P.B. 5818 Patentlaan 2
NL - 2280 HV Rijswijk
Tel. (+31-70) 340-2040, Tx. 31 651 epo nl,
Fax: (+31-70) 340-3016

Authorized officer

Tarrida Torrell, J

INTERNATIONAL SEARCH REPORT

information on patent family members

International Application No

PCT/US 97/17790

Patent document cited in search report	Publication date	Patent family member(s)	Publication date
WO 9613872 A	09-05-96	US 5525436 A AU 4017595 A EP 0787369 A	11-06-96 23-05-96 06-08-97
US 4664761 A	12-05-87	NONE	
US 4693824 A	15-09-87	NONE	
US 5599639 A	04-02-97	JP 9073908 A	18-03-97